



Original Paper

Importance of conformance control in reinforcing synergy of CO₂ EOR and sequestration



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ABSTRACT

Injecting CO₂ into hydrocarbon reservoirs can enhance the recovery of hydrocarbon resources, and simultaneously, CO₂ can be stored in the reservoirs, reducing considerable amount of carbon emissions in the atmosphere. However, injected CO₂ tends to go through fractures, high-permeability channels and streaks present in reservoirs, resulting in inefficient hydrocarbon recovery coupled with low CO₂ storage performance. Conformance treatments with CO₂-resistant crosslinked polymer gels were performed in this study to mitigate the CO₂ channeling issue and promote the synergy between enhanced oil recovery (EOR) and subsurface sequestration of CO₂. Based on a typical low-permeability CO₂-flooding reservoir in China, studies were performed to investigate the EOR and CO₂ storage performance with and without conformance treatment. The effect of permeability contrast between the channels and reservoir matrices, treatment size, and plugging strength on the efficiency of oil recovery and CO₂ storage was systematically investigated. The results indicated that after conformance treatments, the CO₂ channeling problem was mitigated during CO₂ flooding and storage. The injected CO₂ was more effectively utilized to recover the hydrocarbons, and entered wider spectrum of pore spaces. Consequently, more CO₂ was trapped underground. Pronounced factors on the synergy of EOR and CO₂ storage were figured out. Compared with the treatment size, the CO₂ storage efficiency was more sensitive to the plugging strength of the conformance treatment materials. This observation was important for conformance treatment design in CCUS-EOR projects. According to this study, the materials should reduce the channel permeability to make the channel/matrix permeability ratio below 30. The results demonstrate the importance of conformance treatment in maximizing the performance of CCUS-EOR process to achieve both oil recovery improvement and efficient carbon storage. This study provides guidelines for successful field applications of CO₂ transport control in CO₂ geo-utilization and storage.

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1. Introduction

The global demand of oil and gas keeps increasing. At the same

time, “carbon neutrality” strategy has been proposed to solve the global climate change problem. Carbon Capture, Utilization, and Storage (CCUS) is an indispensable way to achieve the “carbon neutrality” target. Injecting CO₂ into oil reservoirs can not only enhance oil recovery (termed as CCUS-EOR), but also realize geological storage of the CO₂, removing a large fraction of CO₂ emissions from the atmosphere. CCUS-EOR has been demonstrated

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an effective and economically feasible way to achieve large-scale CO₂ reduction. China intends to realize the goal of “carbon emission summit” in 2030 and “carbon neutrality” in 2060. To achieve these goals, China’s overall emission reduction demand via CCUS in 2030 will be 2×10^7 – 4.08×10^8 t/a (Zhang et al., 2021). Meanwhile, the geological utilization and storage potential in China is very significant (1.5×10^{12} – 3.0×10^{12} t CO₂ onshore), which can theoretically meet the demand for emission reduction. However, the current CO₂ geological utilization and storage capacity in China is only 1.21×10^6 t/a (Zhang et al., 2021), which is far below the demand for emission reduction. Therefore, enormous potential of geological utilization and storage has not been fully utilized.

Most reservoirs in CCUS-EOR projects in China are featured with low permeabilities (< 50 md) (Qin et al., 2015; Hu et al., 2019). Specifically, 10–50 md is ordinary low permeability, 1–10 md is extra-low permeability, and 0.1–1 md is ultra-low permeability. China is rich in low permeability oil and gas resources, accounting for about 46% of the total reserves of the country. In recent years, low permeability oil reservoirs account for more than 70% of the newly proved reserves (Li, 2020). Injecting CO₂ is an effective way to unlock the low-permeability resources (Huang et al., 2022; Li, 2020; Zhang et al., 2018, 2019). Recently, Liu and Rui (2022a, b) proposed a new concept, named storage-driven CO₂-EOR, which collaborates CO₂-EOR with carbon storage in oil reservoirs to achieve optimal oil recovery and carbon storage simultaneously. It provides a feasible approach to a paradigm shift in hydrocarbon recovery, from a massive-emission process to a net-zero-emission one.

However, fractures and high-permeability channels are usually present in the reservoirs, especially at scales in consideration. Being exposed to such heterogeneities, injected CO₂ tends to channel from injection wells to production wells through the high-permeability streaks and escapes to the surface prematurely, failing to achieve effective geo-storage, with effective storage rates less than 20% (Ye et al., 2021). Seriousness of such gas channeling issues was an important reason to restrain the expansion of CO₂-EOR pilot tests to large scale applications in the 1990s in China (Li, 2020). The channeling problem has not been effectively solved although important theoretical and technical progresses have been made over the years.

Since the commercial applications of CO₂ flooding in the 1970s, a variety of strategies have been developed to control CO₂ channeling, such as water-alternating-gas injection (WAG), mechanical isolation, cement squeeze, gel, foam, and CO₂ thickening (Enick et al., 2012; Qin et al., 2015). The WAG method has been widely used, but it has poor gas-channeling-control ability when the heterogeneity issue is too severe (such as the existence of macroscopic fractures) (Enick et al., 2012; Sun et al., 2020). Polymer gels can seal off the high-permeability features, improve crossflow and effectively inhibit channeling of displacing fluids, which have been widely used in water flooding and chemical flooding (Bai et al., 2013; Seright and Brattekas, 2021; Kang et al., 2021; Zhu et al., 2017; Sun et al., 2020). Polymer gels are expected to selectively block the flow of CO₂, forcing subsequent injected CO₂ fluid to enter the low-permeability zones where the oil saturation is high. As a result, more oil can be recovered and due to the improvement of volumetric coverage, CO₂ can enter into more pore spaces. Therefore, it cannot only improve oil recovery, but also force the CO₂ to enter additional pore spaces and be trapped, improving the CO₂ storage efficiency.

Different gel systems have been developed for conformance control. In-situ polymerization gel systems were applied in early field tests in 1980s (Woods et al., 1986; Martin and Kovarik, 1987). For such gel systems, monomer solutions with crosslinkers were injected into the reservoirs to be treated. *In-situ* polymerization and

crosslinking reactions took place underground to form gels. The gelant was easy to be injected due to the low viscosity, which was close to water. However, the polymerization and gelation reactions were susceptible to formation conditions such as temperature, brine salinity and composition, pH, and shearing. Also, these gel systems could enter and damage the low-permeability zones where remaining oil was present (Seright, 1995, 1997; Seright and Lee, 1999). Another way is to inject polymer solutions containing cross-linking agents (e.g., Cr³⁺). The gelant viscosities are higher, close to polymer solutions. Higher viscosities alleviate the formation damage problem and the shortcomings associated with in-situ polymerization (Seright, 1997; Sydansk and Romero-Zeron, 2011).

In 1990s, Seright studied the conformance improvement performance by injecting preformed bulk gels (PBG) into heterogeneous reservoirs (Seright, 1997). Crosslinking reactions take place and gels are formed before they are injected into reservoirs. The PBG systems overcome some drawbacks associated with in-situ gels. PBGs are proven to be effective to solve fracture-type features in reservoirs (Seright, 1997, 1999a, b, 2001, 2003; Raje et al., 1999; Asghari et al., 1999; Fakher et al., 2018). PBGs have been used in CO₂-flooding projects in the United States (Hild and Wackowski, 1998) and the Middle East (Karaoguz et al., 2004). However, PBGs are difficult to achieve in-depth profile control due to poor injectivity in smaller fractures or matrix-type channels. Experiments showed that the required injection pressure gradient would exceed 200 psi/ft even when the permeability of matrix type channels was up to 27 darcies (Seright, 1999a). Such a high-pressure gradient is only found within a few feet around a wellbore. In the late 1990s, millimeter-sized preformed gel particles (PPG) were developed for in-depth conformance control. PPGs were successfully applied in Zhongyuan Oilfield and were rapidly promoted thousands of wells (Coste et al., 2000; Bai et al., 2008, 2015). PPGs effectively overcome some drawbacks of in-situ gels and PBGs (Bai et al., 2015; Dai et al., 2017; Kang et al., 2021).

Since CO₂ is acidic and corrosive, different polymer gel systems have been developed to improve their CO₂-resistance capacity (Sun et al., 2020; Kang et al., 2021; Li et al., 2016). Lashari et al. (2019) studied macroscopic and microscopic rheological properties of composite gels used for CO₂ flooding conformance control. The addition of SiO₂ enhanced the water-holding capacity of the gels. Thereby, reducing the severity of dehydration of the gels under exposure to CO₂. Fakher et al. (2018) evaluated the plugging performance of HPAM gel under supercritical-CO₂ conditions, and found that the plugging ability of HPAM gel was insufficient when they were exposure to supercritical CO₂, especially under low-salinity conditions. Geng et al. (2019) and Ding et al. (2020) developed a pH-responsive nano/submicron-PPG copolymerized with PAM-AA. The effects of monomer type, crosslinker concentration and pH value on the physicochemical properties of gel particles were investigated. The physicochemical properties include morphology, Zeta potential and hydrodynamic diameter, and the mechanism of pH response of the gels. Pickering emulsions with additions of the nano/submicron-PPGs were found to be stable under low pH (acidic) conditions. Zhao et al. (2021), and Zhao and Bai (2022a, b, c) evaluated the selective plugging mechanism of micrometer-sized gel particles in heterogeneous reservoirs with super-permeable channels. Kang et al. (2021), Sun et al. (2020) and Zhu et al. (2017) summarized gel systems for conformance control.

However, unlike traditional CO₂-EOR projects, which are driven by the single goal of enhanced hydrocarbon resource recovery, CCUS-EOR projects are driven by multiple goals: enhanced hydrocarbon resource recovery, and optimal CO₂ geo-storage at the exit. Therefore, the requirements for conformance control in traditional CO₂-EOR projects and CCUS-EOR projects are also different. With an increasing emphasis on CO₂ reduction especially in recent years,

more attention should be paid to the synergy of CO₂ EOR and sequestration. Conformance control of CO₂ flow in reservoirs is crucial to achieve the synergistic performance. Such studies are still highly scarce. This work intended to study the effect of conformance control in reinforcing the synergy with oil recovery and CO₂ storage. The impact of conformance channel permeability, treatment size, and plugging strength was systematically studied. Favorable conditions for reinforcing the synergy of CO₂ EOR and sequestration in low-permeability fractured reservoirs were discussed.

2. Methodology

A conceptual one-layer reservoir model with sealed boundaries was established based on published data of a CO₂-flood reservoir in H-95 block in Jilin Oilfield (Wang, 2013; Ren et al., 2011; Zhang et al., 2016). Particularly, Wang (2013) carried out systematic tests of the fluid properties and CO₂-oil interaction of this block. The published test results provide basis for this numerical simulation study. The model grids were 104 × 104 × 1 with a grid size of 3 m × 3 m × 10 m. The shape of all the grids is uniform. The reservoir dimension was 312 m × 312 m × 10 m. Corner-point grid system was used in the reservoir model. The grid sizes in the x and y directions were small enough to represent the channels and matrices of the reservoir. The grid size in the z direction was a little bit large (10 m) and there was only one layer in the model. This was in accordance with the assumption of “no gravitational override” of the injected CO₂. Meanwhile, coarsening grids appropriately can shorten the operation time to some extent, so the calculation efficiency could be improved.

The reservoir was developed by two parallel horizontal wells with an in-between well distance of 300 m. The horizontal length of the wells was 300 m. The reservoir matrix permeability was 3 md. The horizontal laterals of the wells lay in the middle of layer. The two horizontal wells located near the closed boundary to guarantee the direction of CO₂ was from the injection well to production well and fully utilized the driving energy of CO₂. Horizontal wells were adopted to take advantage of their advantages. As the reservoir model was consisted with a thin layer, vertical wells were not efficient to extract the hydrocarbon resources. By contrast, horizontal wells had a much larger contact area with the reservoir to develop the crude oil and inject and sequester CO₂ more efficiently. Also, the choice was in accordance with field practice as horizontal wells were used widely in extra-low permeability reservoirs to enhance the injectivity and productivity and ensure an economic injection rate and oil production rate.

High-permeability streaks and fractures were present in the reservoir. Three high-permeability channels with a width of 9 m were introduced to represent the streaks and fractures. The channels connected the injector and producer. The permeability of the channels depends on the cases to be researched. The reservoir model is shown in Fig. 1. The oil composition is summarized in Table 1. The basic data of fluids and reservoir was shown in Table 2. Table 3 and Table 4 present the PVT properties of the crude oil-CO₂ systems. The initial oil saturation was 0.56. Relative permeabilities of oil, water and CO₂ were shown in Fig. 2. The dataset of relative permeability is gained by a series of core experiments and normalized by Eclipse-SCAL software (Wang, 2013). Gel treatment was performed to seal off the channels. The channel permeability in each case study was specified in Table 5. The impact of treatment size, channel permeability, plugging strength on oil recovery and CO₂ storage performance was investigated through a series of case studies. The following assumptions were introduced in the simulation studies.

- (1) The matrix of the reservoir was homogenous and isotropic;
- (2) The temperature of the reservoir was uniform in each grid and kept constant during production. The flowing of fluid in the reservoir was assumed to be isothermal;
- (3) The migration of CO₂ in the reservoir due to the buoyant force was ignored. That is, it was assumed there was no override of the injected CO₂. The fluid saturation distribution in the vertical direction was the same. This assumption was reasonable considering the small thickness of the reservoir.
- (4) The two horizontal wells were located near the closed boundaries to guarantee the direction of CO₂ is from injection well to production well and fully utilize the driving energy of CO₂;
- (5) The gel materials were assumed ideally placed in the pre-calculated position of the high-permeability channels without entering other position in the reservoir;
- (6) Ignore the reaction of CO₂ with matrix or gel materials.

It should be noted that transport and placement of gel materials in fractures and matrix-type high-permeability channels are complex processes. Physical processes that are involved in are dehydration, leak-off, particle breakage, rheological behavior, disproportionate permeability reduction, inaccessible pore volume, CO₂-response behavior and etc. Detailed discussions on some of these topics can be found in the literature (Bai et al., 2013; Zhao et al., 2021; Zhao and Bai, 2022a, b, c; Seright, 1997; Seright and Brattekas, 2021; Willhite et al., 2002; Zhang and Bai, 2011; Imqam et al., 2017; Leng et al., 2021; Dai et al., 2017; Song et al., 2018; Sun and Bai, 2017; Sun et al., 2020, 2021; Wang and Bai, 2018). To make our study focused without going into the theoretical detail of the complex transport and placement processes of gel materials that are already covered in the already cited literature, we substantially simplified and scaled the treatment processes in the numerical studies. The gel materials selectively placed in the high-permeability channels without entering the reservoir matrices. The plugging ability of the materials could be maintained over the lifespan of reservoir development. In reality, the plugging ability tended to gradually diminish as more displacing fluid was injected and flowed through the reservoir. However, it could be remedied by being re-treated with gel materials. Also, the permeability reduction capacity was assumed the same to different fluids. Without getting into more complex treatment processes, we put our focus on the key questions of 1) what a conformance treatment is required in order to achieve synergy of CO₂ EOR and geo-sequestration, and 2) key parameters and favorable conditions for conformance treatment to reinforce the synergistic outcomes.

3. Results and discussion

Fifteen sets of numerical simulations were performed to investigate the effect of permeability contrast (K_c/K_m), relative treatment size (L_t/L_c), and plugging strength (K_c/K_c') on oil recovery performance and CO₂ storage efficiency. The results are discussed in subsequent sections.

3.1. Effect of conformance control on EOR and CO₂-storage

In the base case (case 0), CO₂ flooding was performed without gel treatments. the CO₂ broke through after 160 days and a significant portion of oil was bypassed (see Fig. 3). Also, lower CO₂ saturation was observed in the bypassed areas. To improve the oil recovery and CO₂ storage, in case 1, gel treatment was performed to seal off the channels. Half length of the channels was sealed off by CO₂-resistant polymer gels (relative treatment size = $L_t/L_c = 1/2$). The channel permeabilities were reduced by a factor of 100

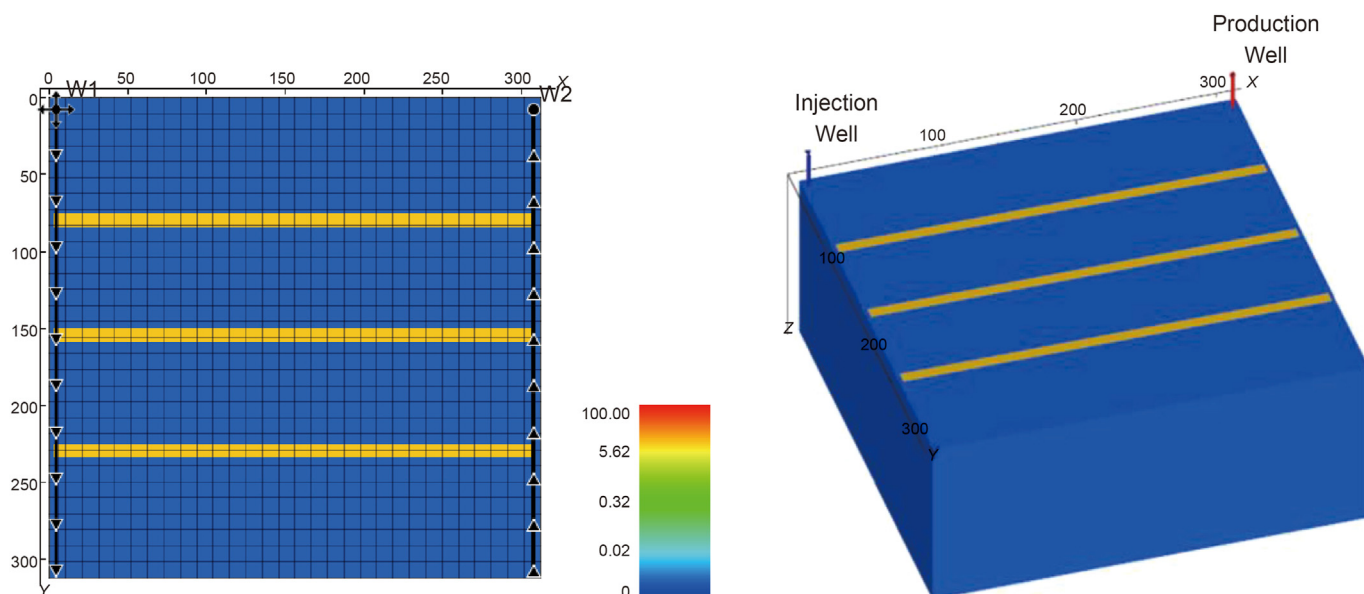


Fig. 1. 2D and 3D view of reservoir model (permeability in darcy).

Table 1
Oil composition (Wang, 2013; Ren et al., 2011; Zhang et al., 2016).

| Components | Fraction, mol% | Fraction, wt% |
|-----------------|----------------|---------------|
| CO ₂ | 0.1 | 0.02 |
| N ₂ | 2.62 | 0.42 |
| C ₁ | 16.46 | 1.51 |
| C ₂ | 4.29 | 0.74 |
| C ₃ | 3.24 | 0.82 |
| iC ₄ | 0.49 | 0.16 |
| nC ₄ | 1.92 | 0.64 |
| iC ₅ | 0.69 | 0.29 |
| nC ₅ | 1.88 | 0.78 |
| C ₆ | 2.99 | 1.44 |
| C ₇₊ | 65.32 | 93.18 |
| Total | 100 | 100 |

Note: Relative density and MW of C₇₊ was 0.8437 and 230 respectively.

(plugging strength, quantified with Residual Resistance Factor, $RRF = 100$). For comparison, another case study was performed in which no gel treatment was performed (case 0). Detailed information of the model variants was summarized in Table 5 along with Table 2 for basic data. The oil recovery performance and CO₂ storage efficiency with and without gel treatment were shown in Figs. 3–5.

As expected, the CO₂ broke through the reservoir quickly when high-permeability channels were present in the reservoir. The CO₂ breakthrough was delayed after gel treatment from 160 days to 220 days (Fig. 4). As seen in Fig. 3c and g, the remaining oil saturation was located between the channels. The swept area was obviously increased after conformance treatment. The area with high remaining oil saturation was decreased. The injected CO₂ was diverted to the remaining oil region to displace the bypassed oil due

Table 2
Basic parameters (Wang, 2013; Ren et al., 2011; Zhang et al., 2016).

| Parameter | Value |
|--|---|
| Grid dimension | 104 × 104 × 1 |
| Grid size | 3 × 3 × 10 m ³ |
| Reservoir dimension | 312 × 312 × 10 m ³ |
| Porosity | 0.1 |
| Initial oil saturation (S_{oi}) | 0.56 |
| Residual oil saturation (S_{or}) | 0.25 |
| Depth | 2160 m |
| Thickness | 10 m |
| Minimum miscibility pressure (MMP) | 22 MPa |
| Reservoir temperature | 95 °C |
| Reservoir pressure | 21 MPa |
| Permeability of matrix (K_m) | 3 md |
| Permeability of channels (K_c) | 10 darcies |
| No. of channels | 3 |
| Bubble point | 7.83 MPa |
| Live oil density | 0.7861 g/cm ³ |
| Dead oil density | 0.8437 g/cm ³ |
| Oil viscosity | 1.79 mPa s |
| Single-stage flash gas-oil ratio (standard conditions), m ³ /m ³ | 34 |
| Original volume factor | 1.1222 |
| Molecular weight of degassed oil | 230 |
| Oil Shrinkage factor (standard conditions) | 11.42 |
| Thermal expansion coefficient | 1.0509 × 10 ⁻⁴ K ⁻¹ |

Table 3
Constant composition expansion experiment data at 95 °C (Wang, 2013; Ren et al., 2011; Zhang et al., 2016).

| Pressure, MPa | Relative volume | Volume factor | Density, g/cm ³ | Viscosity, mPa·s |
|---------------|-----------------|---------------|----------------------------|------------------|
| 22.5 | 0.9785 | 1.1222 | 0.7861 | 1.7904 |
| 20 | 0.9816 | 1.1258 | 0.7836 | 1.7400 |
| 16 | 0.9870 | 1.1319 | 0.7794 | 1.6885 |
| 12 | 0.9930 | 1.1388 | 0.7747 | 1.6036 |
| 8 | 0.9997 | 1.1465 | 0.7694 | 1.5154 |
| 7.83 | 1.0000 | 1.1469 | 0.7692 | 1.4237 |
| 4 | 1.3343 | 1.1143 | 0.7803 | 1.4198 |
| 1 | 4.0212 | 1.0780 | 0.7944 | 1.4915 |
| 0.5 | 8.1654 | 1.0694 | 0.7991 | 1.5521 |
| 0.1 | 49.4073 | 1.0406 | 0.8093 | 1.5617 |

Table 4
Swelling test data for the CO₂-Oil System at 95 °C (Wang, 2013; Ren et al., 2011; Zhang et al., 2016).

| Ratio of injected gas, % | Saturated pressure, MPa | Swelling factor | Volume factor | Ratio of dissolved gas and oil, m ³ /m ³ | Viscosity of oil, mPa·s | Solubility of CO ₂ , m ³ /m ³ | Density of oil, kg/m ³ |
|--------------------------|-------------------------|-----------------|---------------|--|-------------------------|--|-----------------------------------|
| 0 | 7.83 | 1 | 1.1222 | 32.38 | 1.42 | 0 | 769.22 |
| 10 | 9.43 | 1.028 | 1.1540 | 46.80 | 1.39 | 14.42 | 769.14 |
| 20 | 11.27 | 1.064 | 1.1937 | 64.67 | 1.33 | 32.29 | 769.08 |
| 30 | 13.48 | 1.109 | 1.2444 | 87.54 | 1.22 | 55.16 | 769.21 |
| 40 | 16.31 | 1.168 | 1.3110 | 117.96 | 1.09 | 85.58 | 769.98 |
| 50 | 20.46 | 1.248 | 1.4003 | 160.54 | 0.95 | 128.16 | 773.11 |
| 60 | 28.46 | 1.352 | 1.5177 | 224.54 | 0.84 | 192.16 | 785.57 |

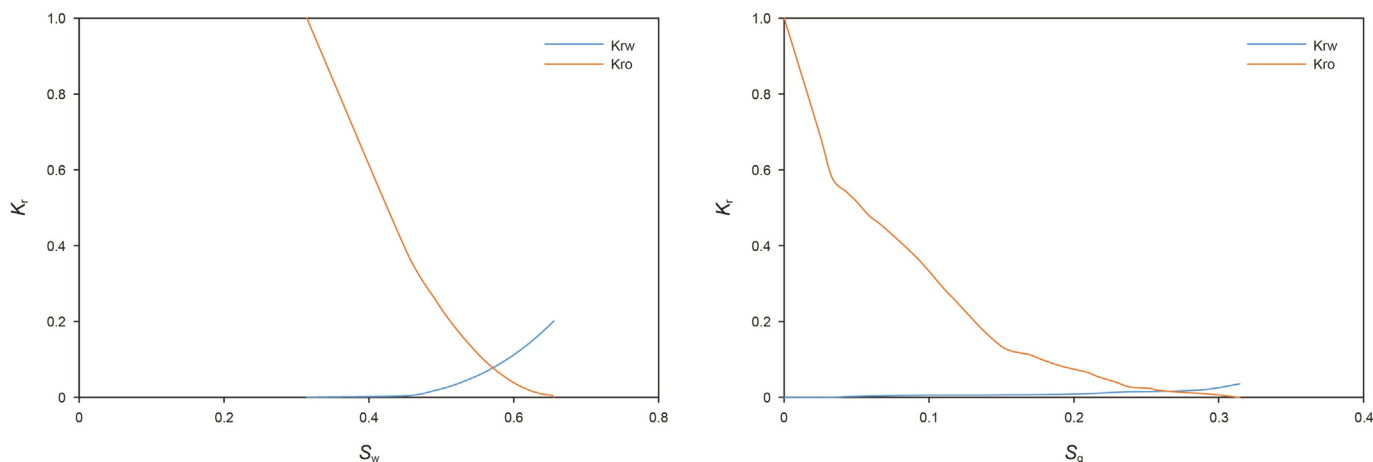


Fig. 2. Relative permeabilities of oil, water and gas (Wang, 2013; Ren et al., 2011; Zhang et al., 2016).

to reservoir heterogeneity. Meanwhile, the CO₂ was trapped in this area, as indicated by high CO₂ saturations shown in Fig. 3d and h. This trapped CO₂ means the CO₂ left in the system and therefore sequestered unless an attempt to be made for its recovery for re-use. After conformance treatments, 6.5% OOIP (0.036 PV) more oil was recovered in 25 years (5.00 PV of CO₂ was injected), and in the first 10 years (1.55 PV CO₂ injection), the oil incremental was 4.8% OOIP (0.027 PV). After breakthrough at the producer, the overall CO₂ storage efficiency kept decreasing. However, the GOR behavior was also improved after conformance treatment. As shown in Fig. 6, GOR increase rate was significantly mitigated with conformance treatment. Accordingly, the dynamic CO₂ storage efficiency, E_s (daily), was increased and resulted in a higher overall CO₂ storage efficiency, E_s (cumulative). After 10 years, the E_s (cumulative) with conformance treatment was 35%, while it was 25% without conformance treatment. Therefore, more CO₂ was left behind in the reservoir.

The results demonstrated that the sweep efficiency was poor

and CO₂ broke through easily when high-permeability channels were present in the reservoir. The storage capacity of the reservoir was not effectively utilized as a significant fraction of the pore spaces were occupied with high-saturation remaining oil. With conformance treatment, the channel permeability was reduced. CO₂ was diverted to the matrix to displace remaining oil. More CO₂ was trapped and stored in the pore spaces and therefore a higher storage efficiency was achieved. The results demonstrated the importance of conformance treatment on oil recovery and resulting CO₂ storage.

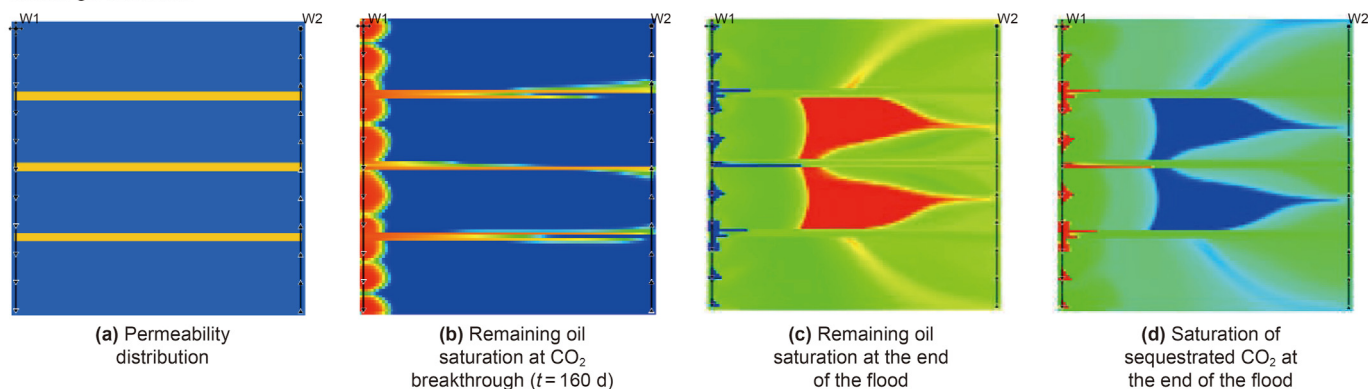
3.2. Effect of channel permeability (permeability contrast)

The effect of channel permeability (and permeability ratio, KR) on the performance of conformance treatment is studied. The channel permeability along with KR represent the severity of heterogeneity of the reservoir. In this study, the heterogeneity was adjusted by changing the channel permeability. The channel

Table 5
Information of case studies.

| Factors | Simulations |
|---|---|
| Without treatment | Case 0 (base case): K_m : 3 md K_c : 10 darcies No. of channels: 3 Gel treatment: not performed |
| Permeability ratio (Channel Permeability K_c) | Treatment size: $1/2 L_c$ Plugging strength: $RRF = 100$ ($K'_c = 1/100$ of K_c) Case 1: $K_c = 10$ darcies Case 2: $K_c = 100$ darcies Case 3: $K_c = 1$ darcies Case 4: $K_c = 0.1$ darcies |
| Treatment size (L_t) | K_c : 10 darcies; Plugging strength: $RRF = 100$ ($K'_c = 1/100$ of K_c) Case 5: $L_t = 1/100 L_c$ Case 6: $L_t = 1/30 L_c$ Case 7: $L_t = 1/5 L_c$ Case 8: $L_t = 2/3 L_c$ Case 9: $L_t = 1/1 L_c$ |
| Plugging strength ($RRF = K_c/K'_c$) | K_c : 10 darcies; Treatment size: $L_t = 1/2$ of L_c Case 10: $RRF = 3$ Case 11: $RRF = 10$ Case 12: $RRF = 30$ Case 13: $RRF = 500$ Case 14: $RRF = 10000$ (i.e., $K'_c = 1$ md) |

Without gel treatment:



With gel treatment:

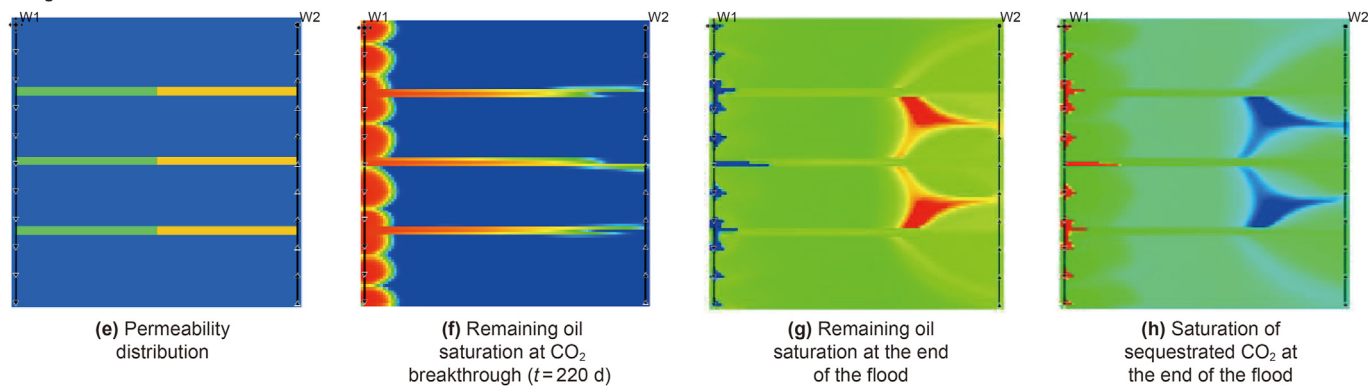


Fig. 3. Results of base case studies with and without gel treatment (color scales are also applied to subsequent cloud plots).

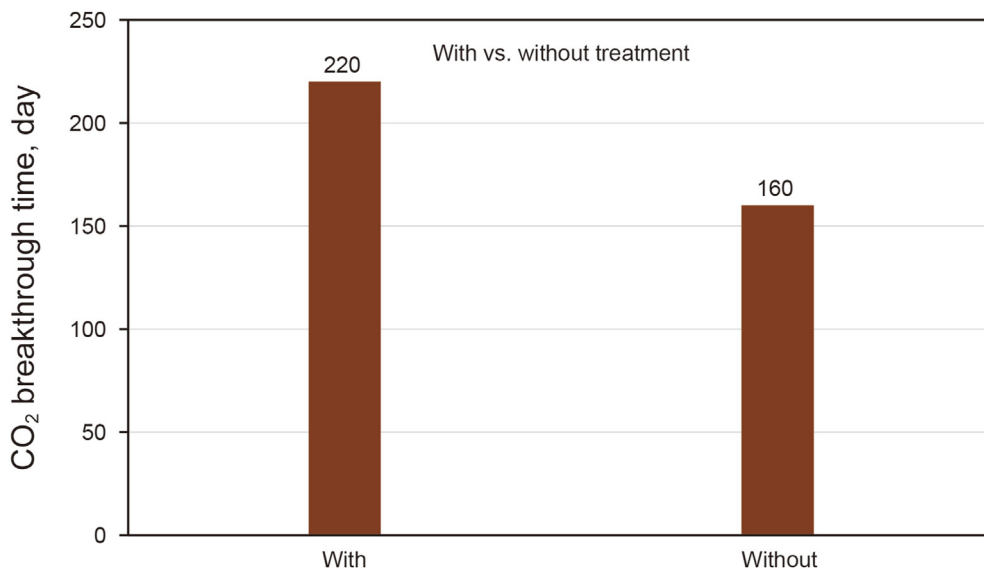


Fig. 4. Comparison of CO₂ breakthrough times with and without gel treatment.

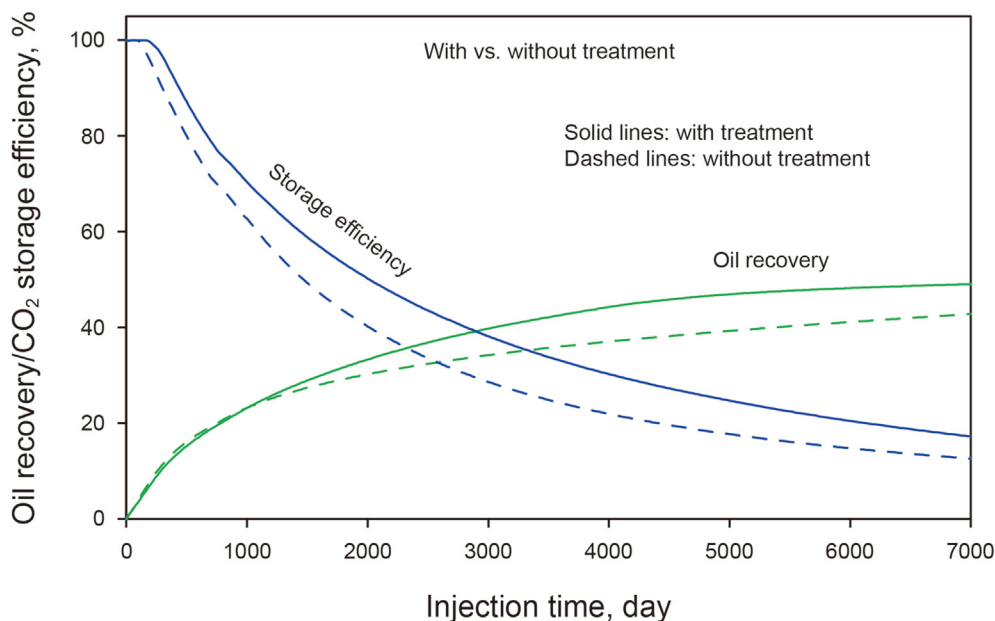


Fig. 5. Comparison of oil recovery performance and CO₂ storage efficiency with and without gel treatment.

permeability was set at 0.1, 1, 10, and 100 darcies, respectively. The results were summarized in Figs. 7–12.

CO₂ breakthrough occurred earlier as the channel permeability increased (Fig. 7). The breakthrough time was 1320 days when the channel permeability was 0.1 darcies (initial KR = 100:3), and decreased to 620 days when the channel permeability reduced to 1 darcies (KR = 1000:3), and 220 days and 180 days when KR = 10,000:3 and 100,000:3, respectively. Note that after gel treatment, the channel permeability and KR were reduced by a factor of 1000:3. After gas breakthrough, producing GOR increased faster, indicating a more severe channeling problem as the reservoir become more heterogeneous. A closer look at the results (Fig. 7) indicated that as $K_c/K_m < 10$, the existence of high-k streaks had a negligible impact on the breakthrough time. This behavior could be explained with the concept of flow capacity. Due to the

small cross-sectional area of the channel systems compared with the entire reservoir, the flow capacity ($K_c A_c$) and the effect of fractures on the channeling problem are limited. The effect of channels become pronounced when K_c/K_m increased over 1000:3. The impact of channels on breakthrough time levelled off when the KR was too large ($K_c > 10$ darcies, and $KR > 10000:3$). The less sensitive trend was due to the extremely severe heterogeneity (super-high channel permeability) (Figs. 8 and 9). The oil recovery improvement was more significant when the KR was increased (Fig. 10). That is, the conformance treatment had a better chance to improve the oil recovery performance when the heterogeneity problem was more serious. The KR also impacted the GOR behavior (Fig. 11). After CO₂ breakthrough, the GOR increases more quickly as KR was larger. The increase trend is similar and the impact of KR become less significant when $KR < 1000:3$. This effect was more clearly

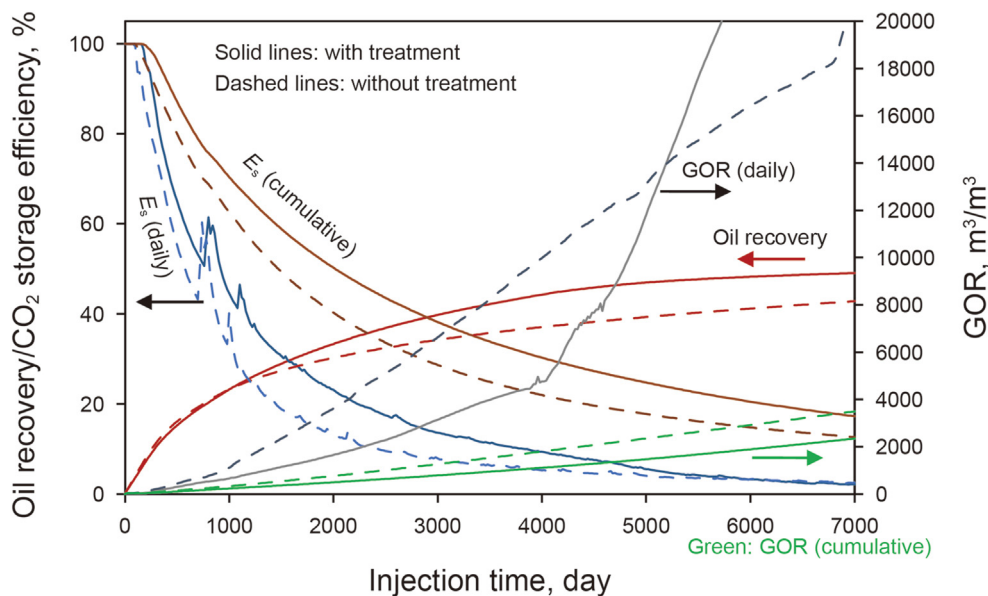


Fig. 6. Comparison of oil recovery performance and CO₂ storage efficiency with and without gel treatment.

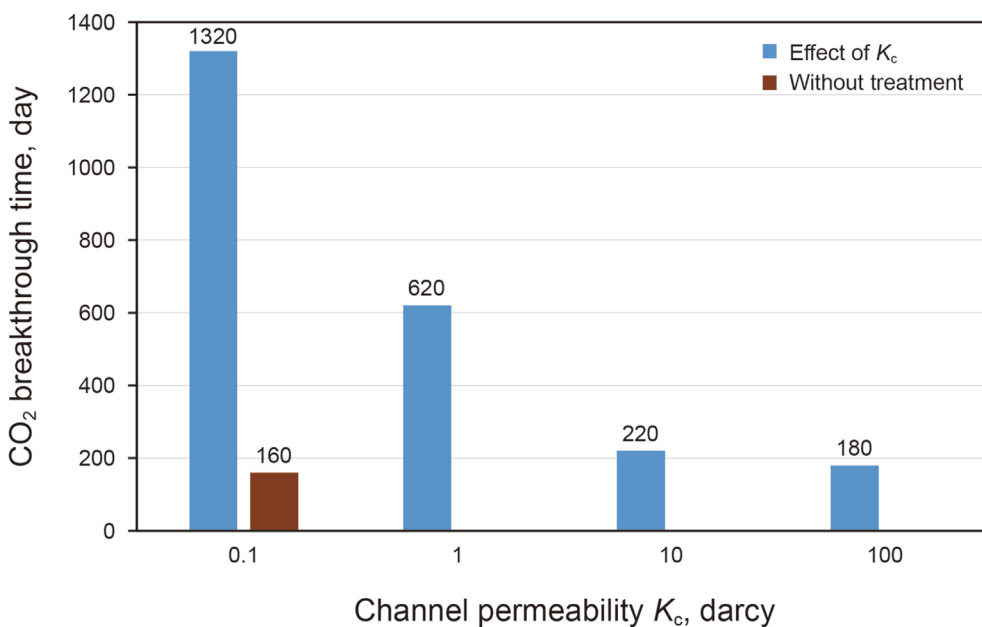


Fig. 7. Breakthrough times of injected CO₂.

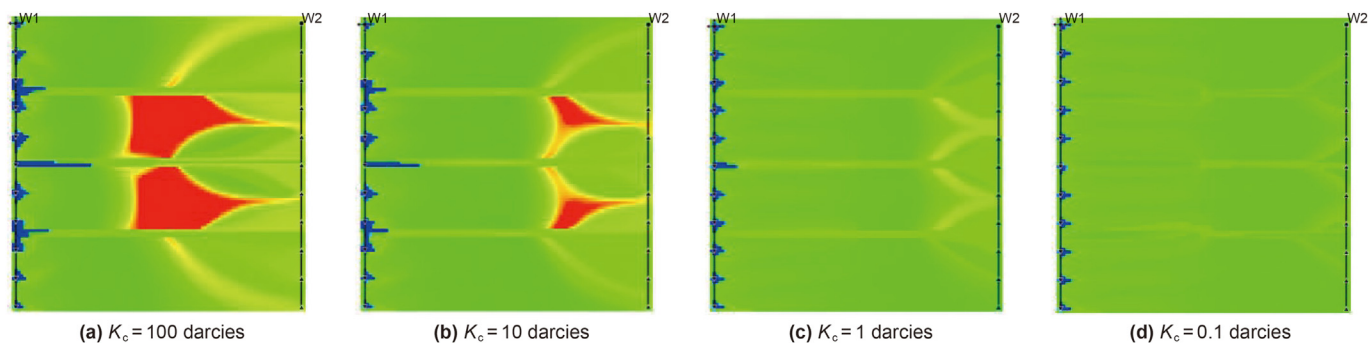


Fig. 8. Effect of channel permeability (K_c) on remaining oil saturation distribution.

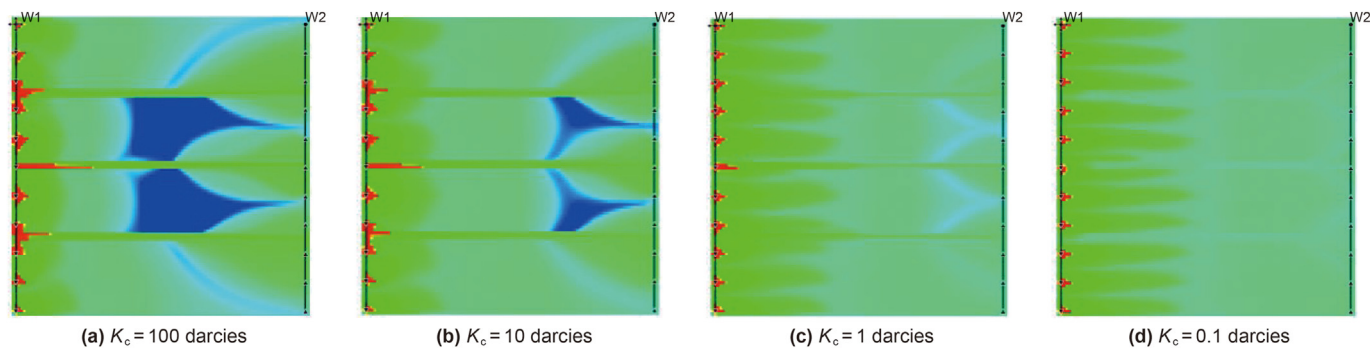


Fig. 9. Effect of channel permeability (K_c) on saturation distribution of sequestered CO_2 .

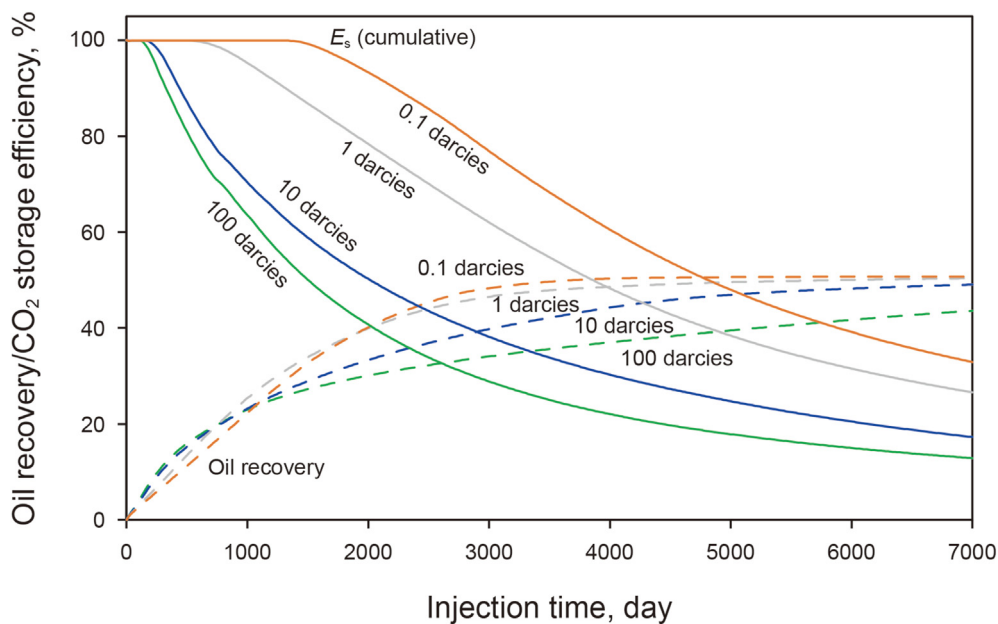


Fig. 10. Effect of channel permeability (K_c) on oil recovery and CO_2 storage.

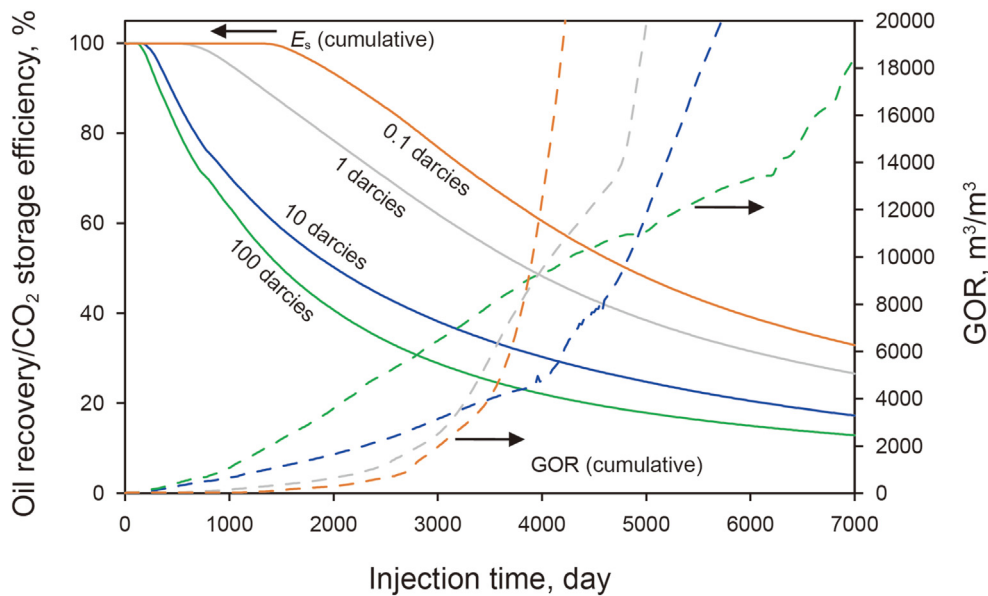


Fig. 11. Effect of channel permeability (K_c) on daily GOR and CO_2 storage.

demonstrated in Fig. 12.

More importantly, compared with the oil recovery performance, the CO₂ storage efficiency was more sensitive to KR (Fig. 10). This behavior has crucial implications on the application of CO₂-EOR, as carbon sequestration plays a more important role according to the zero-emission target. The storage efficiency reduced more rapidly as the channels were more permeable. A higher CO₂ storage efficiency could be achieved when the reservoir was more homogeneous. Conformance treatment was necessary to suppress the channeling of CO₂ through the high-k streaks. After the channels were sealed off, the injected CO₂ was forced into the matrices of the reservoir to displace the remaining oil. Meanwhile, more CO₂ was trapped in the pore spaces of the matrices. Therefore, the storage capacity and efficiency were increased.

3.3. Effect of treatment size

The effect of treatment size on oil recovery and CO₂ storage was also studied. Treatment size was quantified with the relative distance of the channel treated against the total channel length. The treatment size was set at 1/100 L_c, 1/30 L_c, 1/5 L_c, 1/2 L_c, 2/3 L_c, and L_c. The results were summarized in Figs. 13–18. Unswept area of the reservoir slightly decreased when the treatment size was increased from 1/100 L_c to 1/5 L_c, as indicated by the red area in Fig. 13. The unswept area was obviously diminished when the treatment size was increased to 1/2 L_c. Meanwhile, the CO₂ breakthrough was delayed, from 160 days to 220 days with a treatment size of 1/2 L_c (see Fig. 14). The sweep efficiency of the injected CO₂ was increased, and a higher oil recovery was achieved, leading to higher CO₂ occupancy of the pore space. Accordingly, as seen in Fig. 15, the CO₂ saturation was increased, resulting in higher CO₂ storage efficiency, as proven in Figs. 16 and 17. Compared with the permeability contrast, the impact of treatment size on CO₂ breakthrough time was mild. However, the treatment size had a significant impact on the GOR behavior and CO₂ storage efficiency. As shown in Fig. 18, the GOR increased much more rapidly when the treatment size was insufficient, and accordingly, storage efficiency of CO₂ was decreased. The reason was that the gel bank was not large enough to resist the CO₂ flow in high-permeability areas. Thus, the

subsequently injected CO₂ could flow back into the channels and circulate to the producer instead of displacing the remaining oil (see Fig. 14). Therefore, to achieve a satisfactory CO₂ storage efficiency, treatment size should be large enough, at least 1/2 L_c in this study. The results demonstrated the importance of in-depth conformance control for effective CO₂ geological storage, while short-distance near-wellbore treatment was insufficient to mitigate CO₂ channeling. Nano-/micrometer-sized particle gels have the ability to propagate deep into reservoirs to achieve in-depth conformance control. In field practice, inter-well chemical tracer tests were often performed to assist in evaluating the channel size.

3.4. Effect of plugging strength

The effect of plugging strength of the conformance treatment materials on CO₂ channeling, oil recovery, and carbon dioxide storage was studied. Plugging strength was quantified with the residual resistance factor (RRF). The RRF was set at 3, 10, 30, 100, 500, and 10,000. The other parameters were kept the same. The results were summarized in Figs. 19–24.

As shown in Fig. 19, breakthrough times were close to each other when RRF was below 100. The delay in breakthrough was small, from 180 days to 220 days. Note that at the beginning, the initial KR was 10,000:3. The KR was reduced to 10 when RRF = 100. The results suggested that in order to effectively suppress the channeling issue, the gels should plug the channels and reduce the KR to the level of less than 100:3. The breakthrough time was delayed to 440 days and 1040 days when the RRF was increased to 500 and 10,000, respectively. With the increase of plugging strength, the remaining oil regions kept decreasing, and they almost disappeared when the RRF increased to 500 (KR was reduced from 10,000:3 to 20:3), as seen from Fig. 20. The injected CO₂ was diverted to these regions to displace the remaining oil. Therefore, CO₂ saturation in these regions was increased, as is shown in Fig. 21.

The dashed lines in Fig. 22 exhibited the oil recovery performance at different RRFs. A higher oil recovery was achieved when the RRF values were higher. The results were consistent with the observations in Figs. 20 and 21. The results demonstrated that conformance treatments were effective to improve the oil recovery

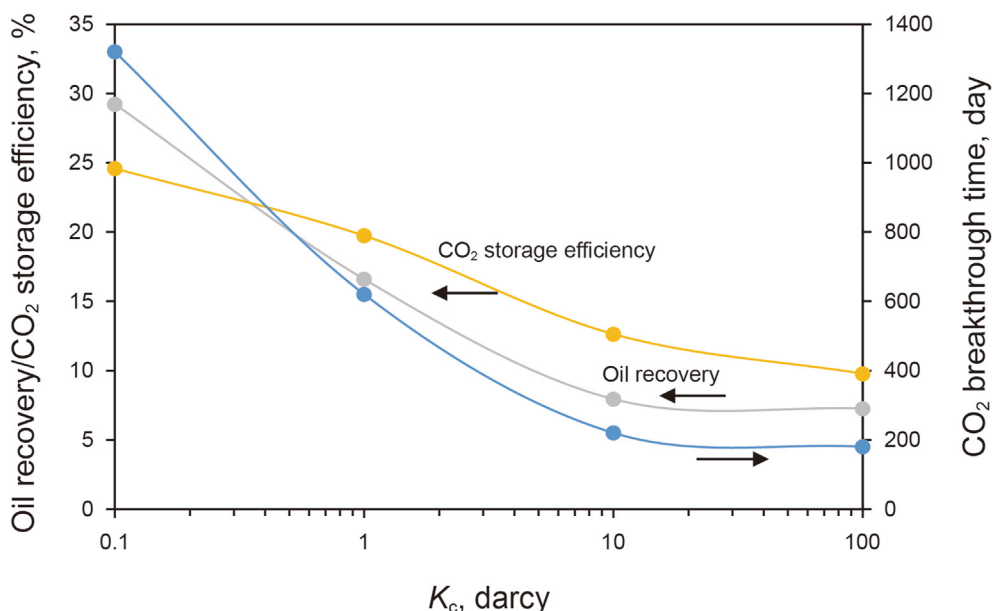


Fig. 12. Impact of channel permeability (K_c) on CO₂ breakthrough, oil recovery and CO₂ storage efficiency.

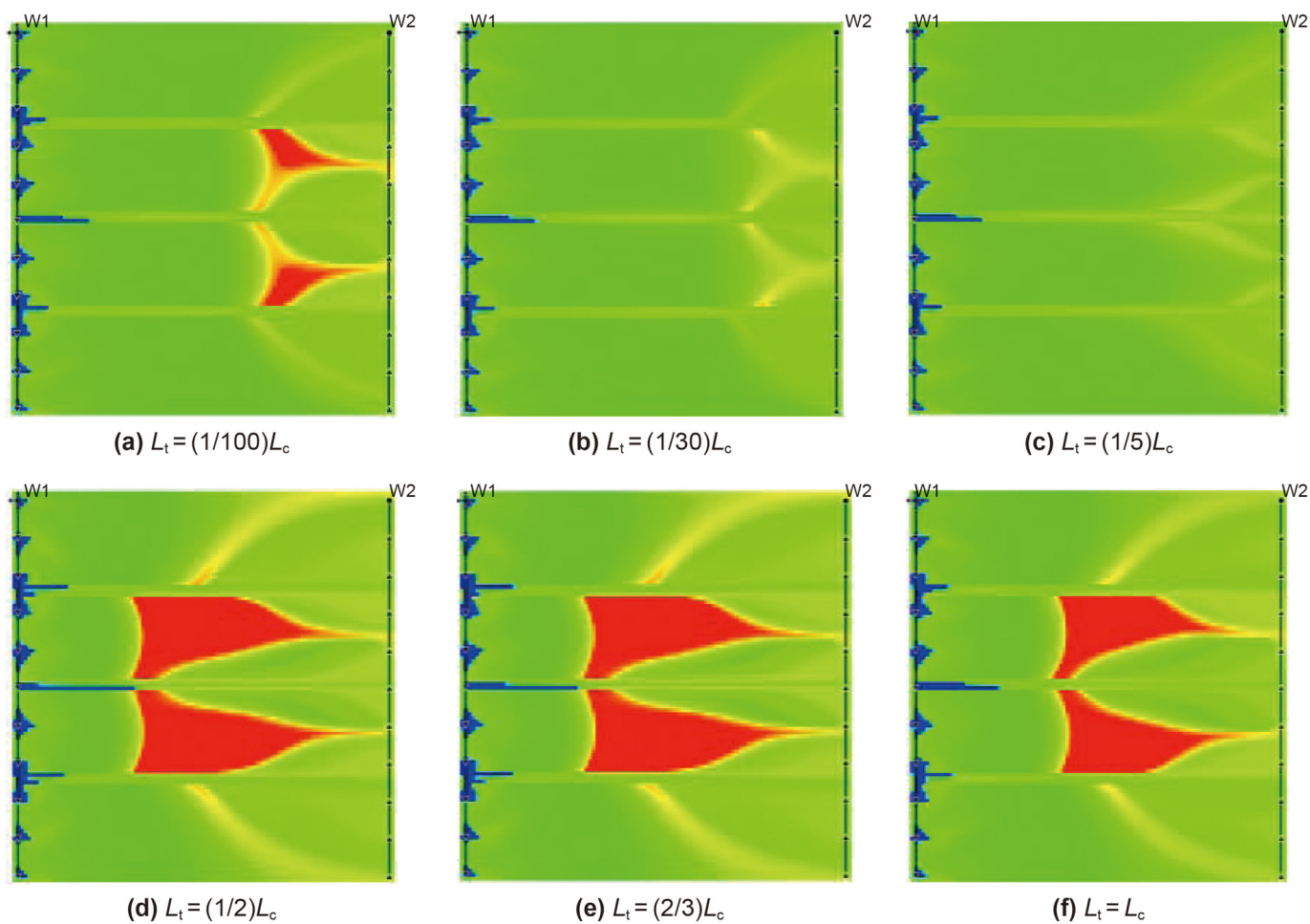


Fig. 13. Effect of treatment size (L_t) on remaining oil saturation distribution.

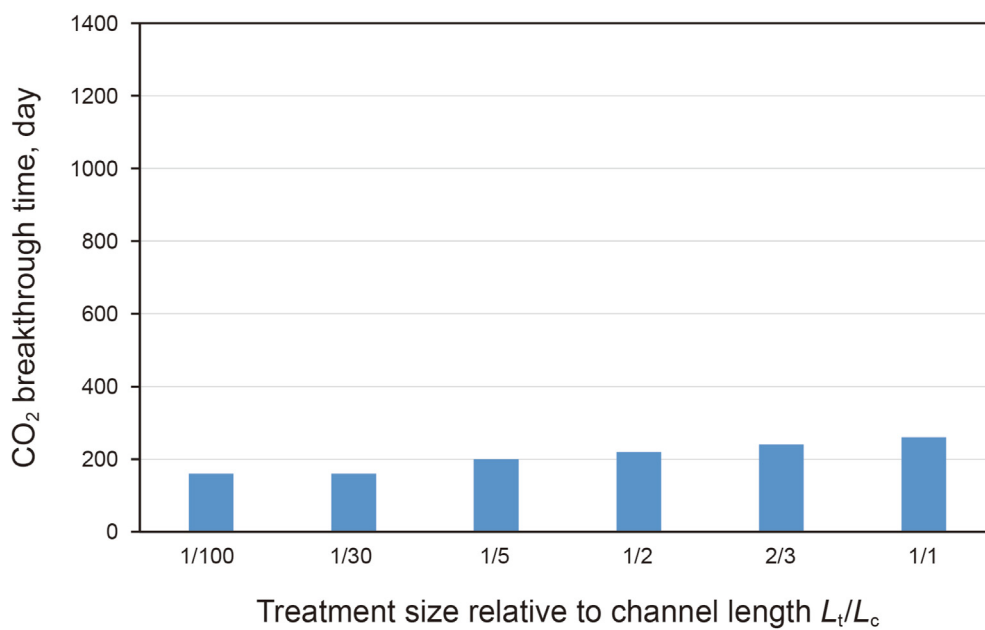


Fig. 14. CO₂ breakthrough times with different treatment sizes.

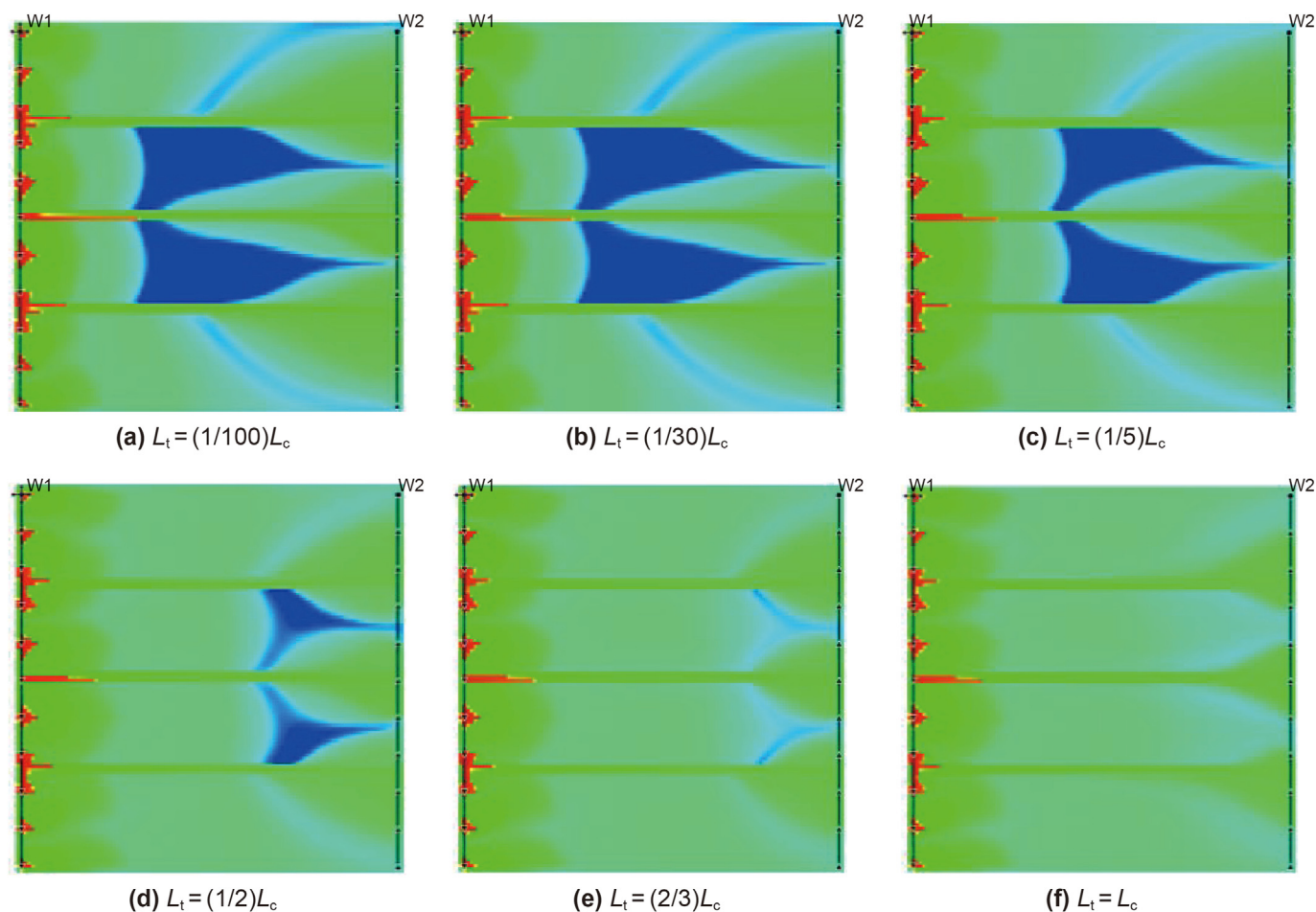


Fig. 15. Effect of treatment size (L_t) on saturation distribution of sequestered CO_2 .

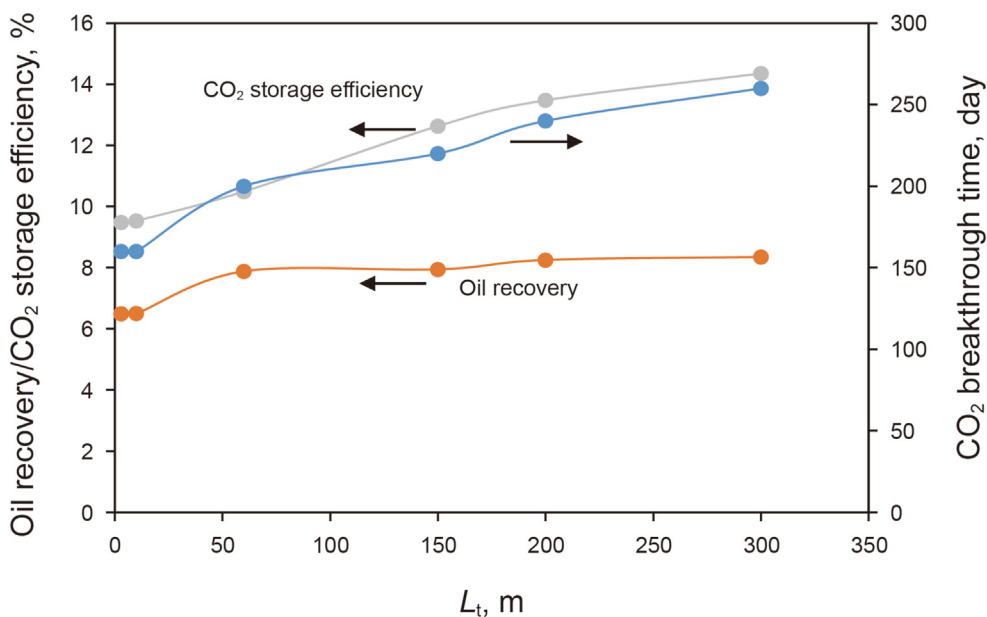


Fig. 16. Effect of treatment size (L_t) on ultimate CO_2 channeling (i.e., represented by breakthrough time), oil recovery and CO_2 storage.

in CCUS-EOR projects. In the case studies, after 10 years, with a conformance treatment of RRF = 500, 10.3% OOIP additional oil was

recovered compared with the case of RRF = 3. When the RRF increased from 3 to 30, the resulting oil recovery improved slightly,

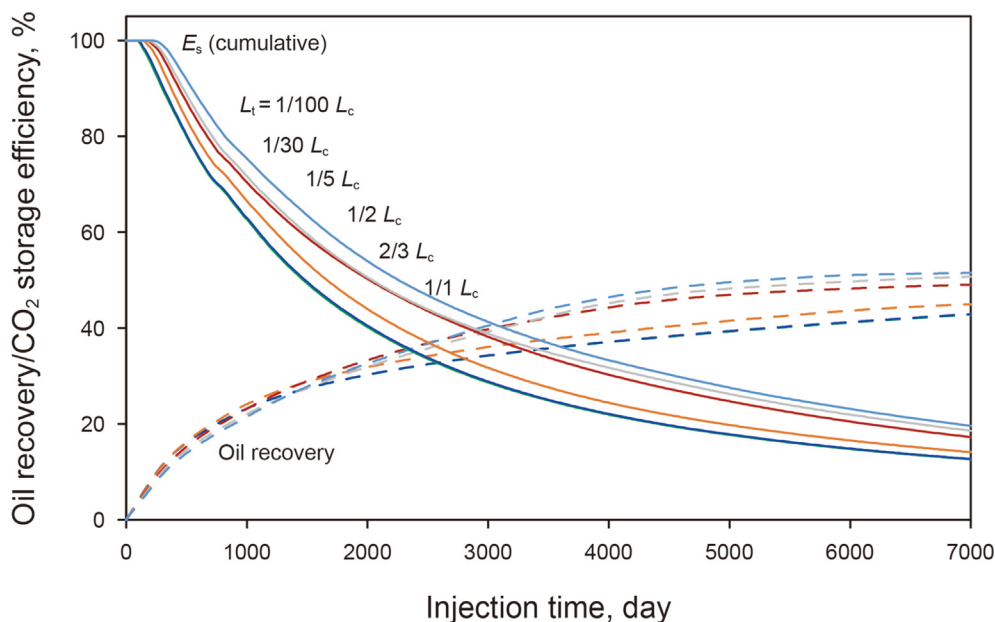


Fig. 17. Effect of treatment size (L_t) on oil recovery and CO₂ storage.

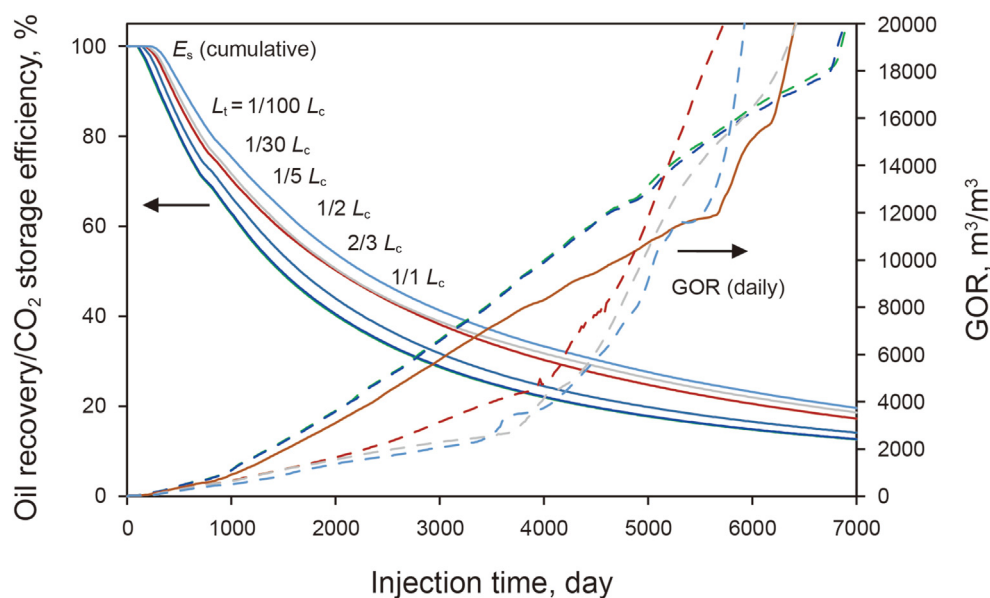


Fig. 18. Effect of treatment size (L_t) on daily GOR and CO₂ storage.

indicating insufficient plugging of the gel materials to the channels. Therefore, the treatment was not effective in terms of the oil recovery improvement. The results clearly indicated the requirement on the plugging strength of conformance treatments to achieve satisfactory oil recovery improvement in CCUS-EOR projects. As shown in Fig. 23 (dashed lines), producing GOR increased faster as the RRF values were lower. Higher GORs were not favorable for oil recovery and CO₂ storage. High GORs indicated poor dynamic CO₂ storage efficiency, as illustrated by the solid lines. The results emphasized the requirement on the RRF to achieve favorable GORs in CCUS-EOR projects. With a higher RRF, a better storage efficiency was achieved. The results in Figs. 21–23 clearly demonstrated that proper conformance treatments could significantly increase the CO₂ storage capacity and efficiency. Variations of the behavior of

CO₂ channeling (breakthrough), oil recovery, and CO₂ storage along with the RRF were also summarized in detail in Fig. 24. A weak treatment (e.g., RRF < 100, KR > 100:3 after treatment) could not effectively address the CO₂ channeling problem. The treatment should establish a sufficient plugging strength (i.e., reducing the channel permeability to an extent of KR below 100:3, ≈30 in this study) to exert a reliable resistance to the CO₂ channeling flow. In field applications, gels could degrade after long-term contact with CO₂ (usually in supercritical conditions). This behavior explains why the RRF was significantly reduced in subsequent cycles during water-alternating-gas (WAG) injection processes. The results of this study emphasized the importance of long-term stability of the conformance treatment materials placed in the channels. The results demonstrate the importance of conformance treatment in

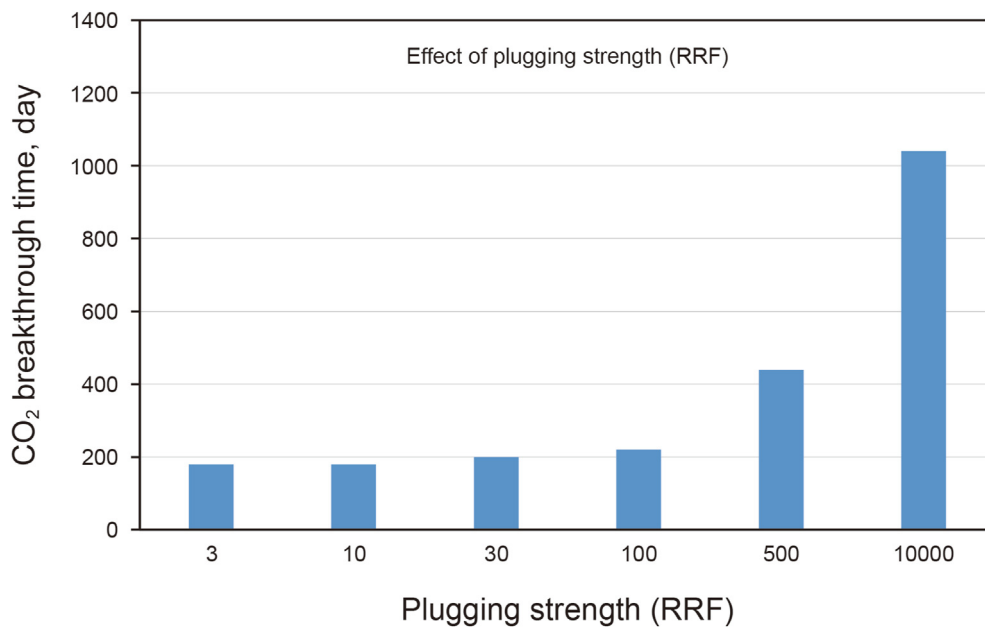


Fig. 19. CO₂ breakthrough times at different plugging strengths.

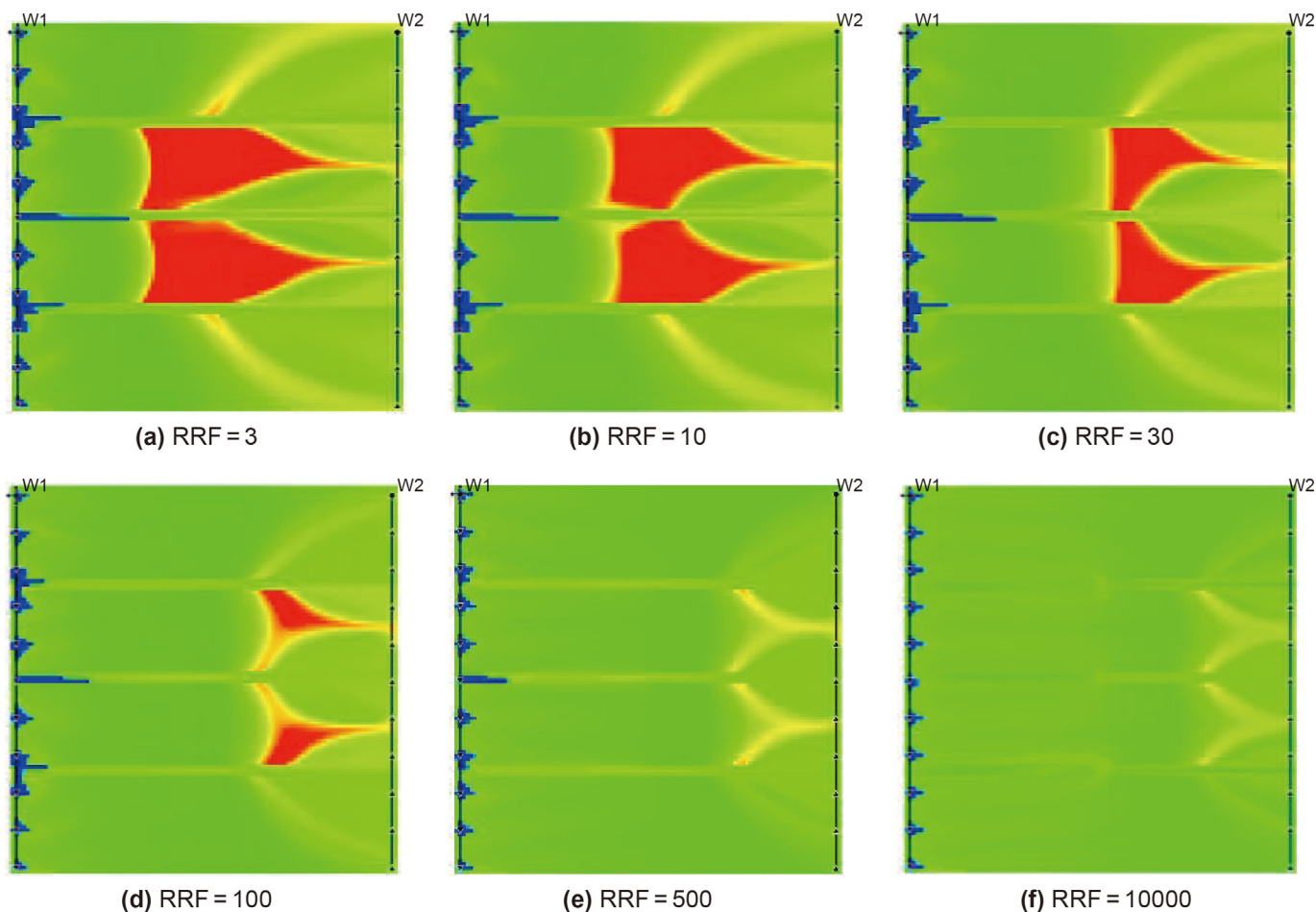


Fig. 20. Effect of plugging strength (RRF) on remaining oil saturation distribution.

maximizing the performance of coupled objectives of CCUS-EOR process to achieve both oil recovery improvement and efficient

carbon storage. Compared with the treatment size, the CO₂ storage efficiency

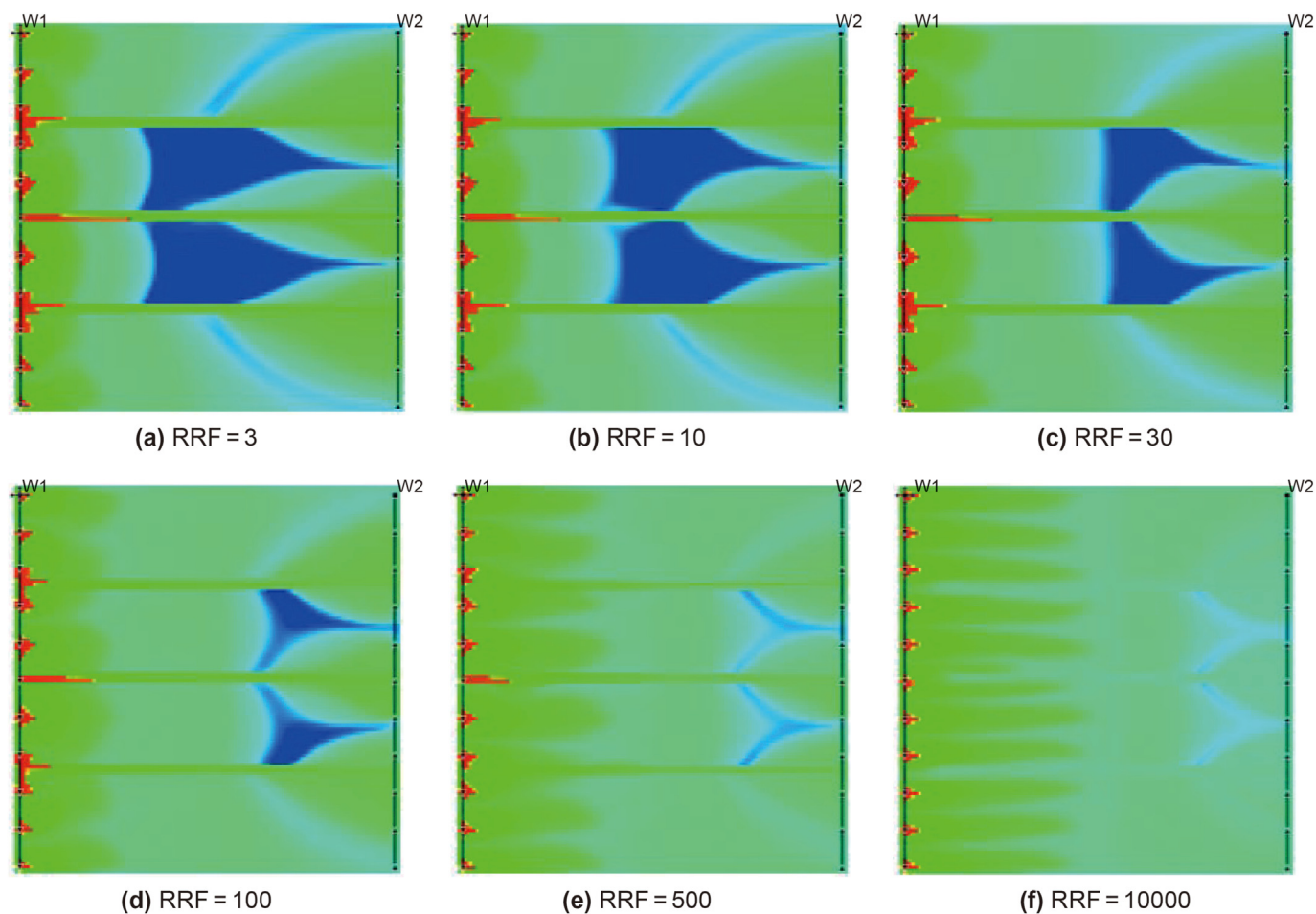


Fig. 21. Effect of plugging strength (RRF) on saturation distribution of sequestered CO₂.

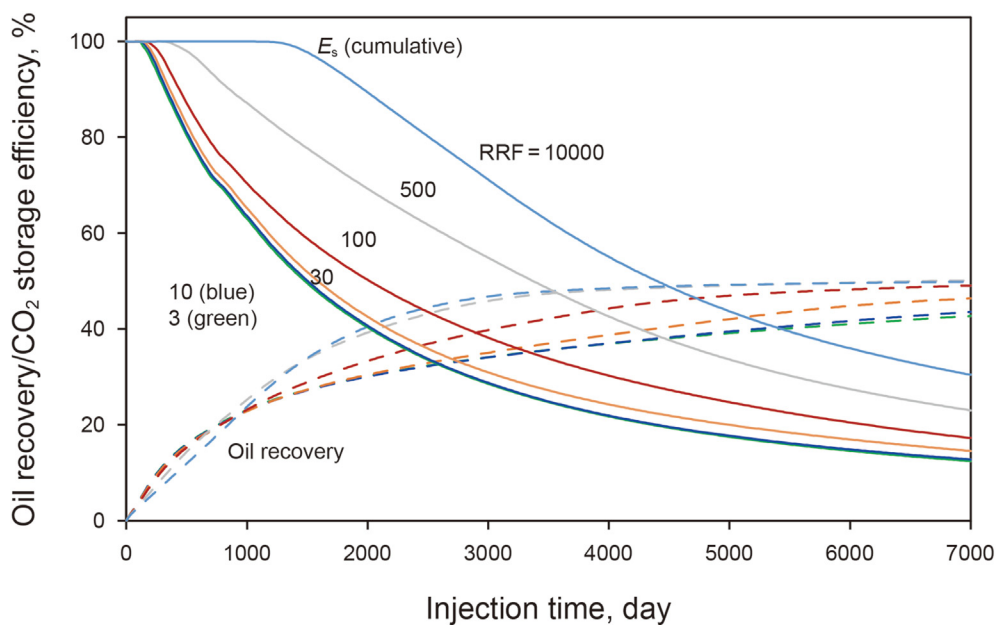


Fig. 22. Effect of plugging strength (RRF) on cumulative oil recovery and CO₂ storage.

was more sensitive to the plugging strength of the conformance treatment materials (Fig. 23 vs. Fig. 19). This observation was

important for conformance treatment design in CCUS-EOR projects. According to this study, the materials should reduce the channel

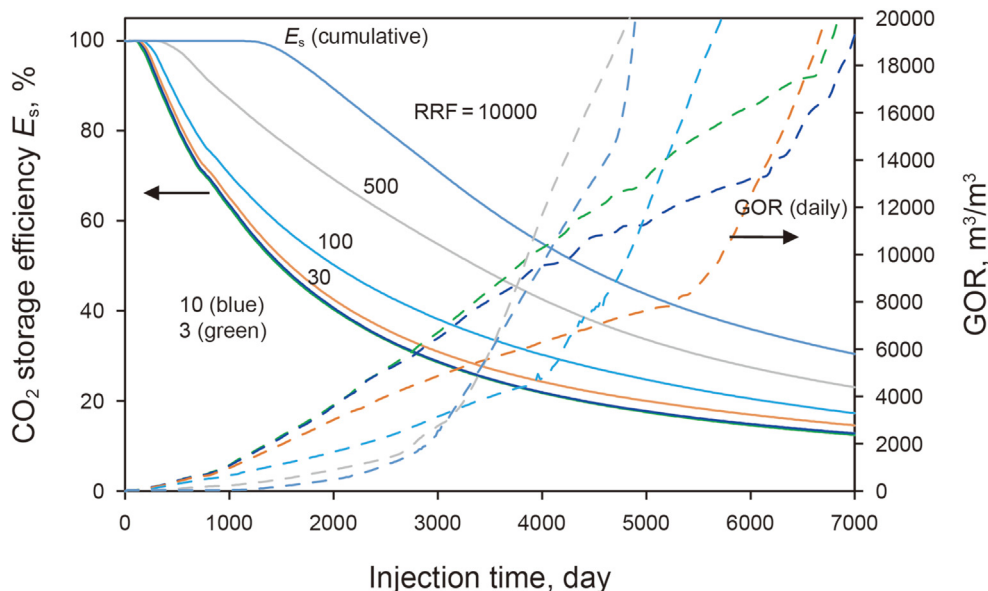


Fig. 23. Effect of plugging strength (RRF) on daily GOR and CO₂ storage.

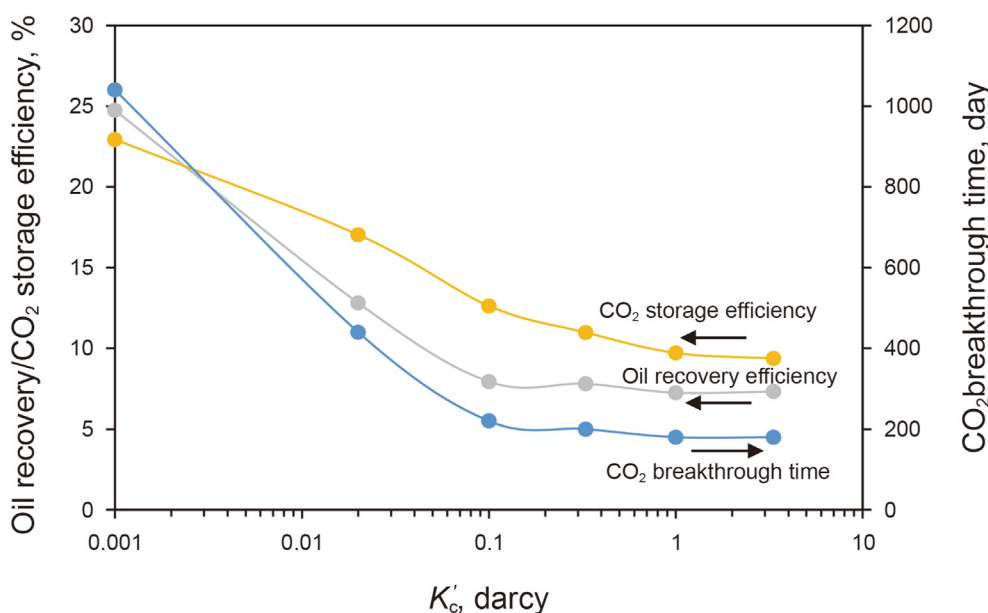


Fig. 24. Effect of plugging strength (RRF) on ultimate CO₂ channeling, oil recovery and CO₂ storage.

permeability to make the KR below 30. In this study, the gel materials were assumed selectively placed in the high-permeability channels without penetrating the reservoir matrices. The selective placement behavior depends on the matching properties between the reservoir and the gels, especially the particle/pore matching size relationship and gel strength. The gels cannot enter the matrices because the pore size of the matrices is too small. Instead, the gel materials can selectively enter the high-permeability channels due to the large pore size in the channels (Zhao and Bai, 2022c). In conformance treatments, attention should be paid to the surface cake and damage to the matrices. The damage could be removed by acid soaking or other chemical and/or mechanical techniques. Thus, we assumed no matrix damage by the gel treatment in this study. Also, attention should be paid to health safety and environmental impact of the treatments. The gel

materials, as in a crosslinked solid state, do not have the ability to migrate to shallow aquifers to contaminate ground water.

The benefits of conformance treatments include delayed CO₂ breakthrough, incremental oil and increased CO₂ storage. Also, the GOR was lowered, reducing the processing cost to separate and recycle the CO₂. A rough economic analysis was performed to evaluate the conformance treatments on CCUS-EOR projects. The economic performance of conformance treatments after 10 years of production in different case studies was summarized in Table 6. In the evaluation, the crude oil price was set at 60 \$/bbl (447.2943 \$/t). The net carbon bonus was set at 50 \$/t. That is, the company could receive a \$50 net bonus when sequestered one ton of CO₂ underground. In the base case (Case 1), the treatment cost was \$200,000. The cost was lower when the treatment size was smaller or the plugging strength was lower. Taking Case 1 (RRF = 100) as an

Table 6
Economic performance evaluation of conformance treatments (after 10 years).

| Factors | Case # | CO ₂ breakthrough time, d | Incremental oil recovery, t | Reduced CO ₂ production, t | Increased CO ₂ storage, t | Benefit from oil gain, USD | Benefit from increased storage, USD | Benefit from reduced CO ₂ production, USD | Treatment cost, USD | Total benefit, USD | |
|------------------------------|-------------------------|--------------------------------------|-----------------------------|---------------------------------------|--------------------------------------|----------------------------|-------------------------------------|--|---------------------|--------------------|----------------|
| With/without treatment | Without | case 0 | 160 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | |
| | With | case 1 | 220 | 4748 | 21958 | 5248 | 2123905 | 262384 | 109791 | 200000 | 2296080 |
| Channel permeability (darcy) | 100 | case 2 | 180 | 2002 | 8509 | 4177 | 895602 | 208873 | 42544 | 150000 | 997019 |
| | 10 | case 1 | 220 | 4748 | 21958 | 5248 | 2123905 | 262384 | 109791 | 200000 | 2296080 |
| | | case 3 | 620 | 6948 | 41537 | 4721 | 3107892 | 236059 | 207685 | 220000 | 3331635 |
| | | case 4 | 1320 | 7726 | 48497 | 4153 | 3455650 | 207652 | 242486 | 250000 | 3655787 |
| Treatment size (L_t/L_c) | 1/100 | case 5 | 160 | 2035 | 7754 | 4365 | 910207 | 218245 | 38770 | 100000 | 1067221 |
| | 1/30 | case 6 | 160 | 2065 | 8142 | 4360 | 923717 | 217984 | 40712 | 120000 | 1062412 |
| | 1/5 | case 7 | 200 | 2815 | 12937 | 4582 | 1259323 | 229089 | 64687 | 150000 | 1403099 |
| | 1/2 | case 1 | 220 | 4748 | 21958 | 5248 | 2123905 | 262384 | 109791 | 200000 | 2296080 |
| | 2/3 | case 8 | 240 | 4962 | 24255 | 4913 | 2219459 | 245660 | 121275 | 250000 | 2336393 |
| | 1/1 | case 9 | 260 | 5477 | 26576 | 4896 | 2449926 | 244785 | 132882 | 300000 | 2527593 |
| | Plugging strength (RRF) | 3 | case 10 | 180 | 1987 | 7646 | 4272 | 888696 | 213601 | 38229 | 130000 |
| 10 | | case 11 | 180 | 1993 | 8422 | 4114 | 891602 | 205695 | 42112 | 150000 | 989409 |
| 30 | | case 12 | 200 | 2592 | 13068 | 4227 | 1159392 | 211361 | 65338 | 180000 | 1256091 |
| 100 | | case 1 | 220 | 4748 | 21958 | 5248 | 2123905 | 262384 | 109791 | 200000 | 2296080 |
| 500 | | case 13 | 440 | 6747 | 36681 | 5357 | 3017697 | 267850 | 183406 | 250000 | 3218953 |
| 10000 | | case 14 | 1040 | 6964 | 46187 | 3797 | 3114836 | 189867 | 230936 | 300000 | 3235638 |

Note: Oil price: 60 \$/bbl = 447.2943 \$/t; Processing cost of produced CO₂: 5 \$/t; Net carbon bonus: 50 \$/t.

example, as mentioned earlier, the CO₂ breakthrough time was delayed from 160 days to 220 days compared with the case without conformance treatments (Case 0). The incremental oil recovery was 4748 t, and the CO₂ storage was increased by 5248 t. Also, 21,958 t of less CO₂ was produced after conformance treatment. The total benefit from the treatment was 2.296 million dollars. The benefits increased with treatment size and plugging strength. The effect of net carbon bonus on the overall economic performance was shown in Figs. 25 and 26. Obviously, the overall benefit increased with the net carbon bonus. A negative value means the company received bonus could not offset the expense to purchase the carbon source. There was even a deficit when the net carbon bonus was too low. The plots can help identify favorable treatment conditions to maximize the economic benefits.

Above all, the results demonstrate that conformance treatment is an effective strategy to help achieve the coupling goal of oil recovery and carbon storage during CCUS-EOR process.

4. Conclusions

The importance of conformance control was systematically investigated to achieve the synergy of enhanced oil recovery (EOR) and CO₂ geo-sequestration. CO₂-resistant polymer gels were introduced to seal off the high-permeability channels and establish in-depth conformance control of the CO₂ flow in reservoirs. The results indicated that after conformance treatments, the CO₂ channeling problem was mitigated during CO₂ flooding and storage. The injected CO₂ was more effectively utilized to recover the

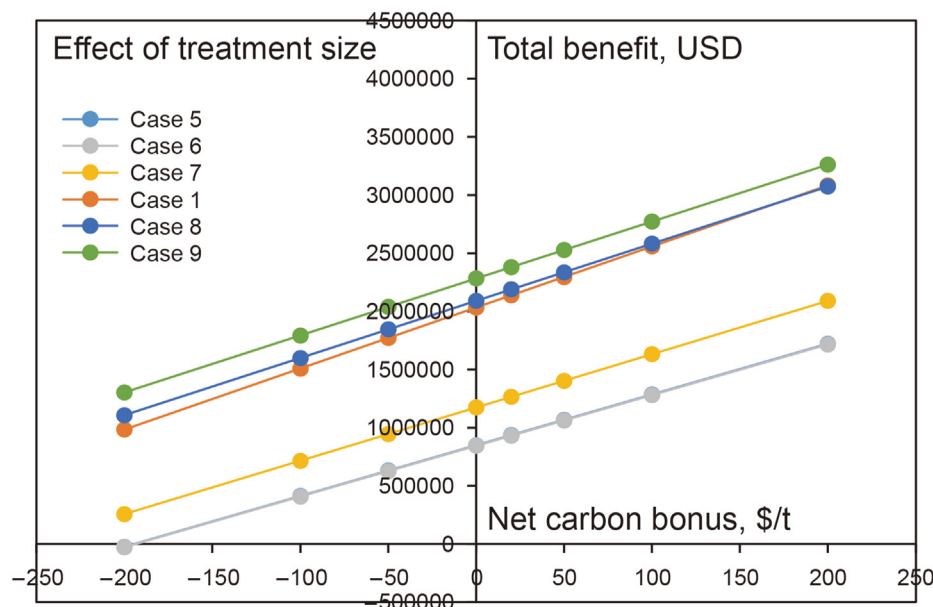


Fig. 25. Effect of treatment size on economic performance at varying net carbon bonus.

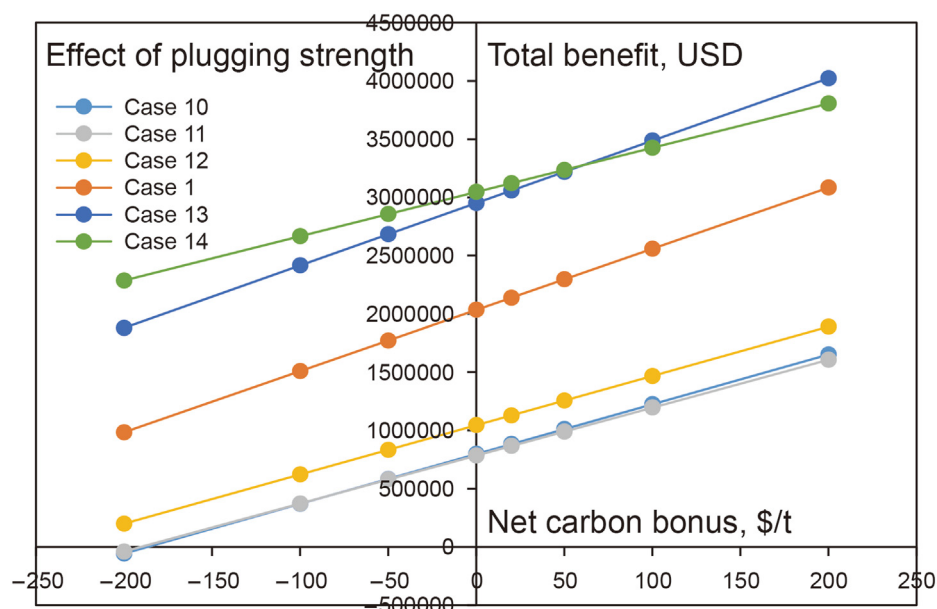


Fig. 26. Effect of plugging strength on economic performance at varying net carbon bonus.

hydrocarbon, and entered more pore spaces. Consequently, more CO₂ was trapped underground. Key parameters on the synergistic objectives of EOR and CO₂ storage were identified. Compared with the treatment size, the CO₂ storage efficiency was more sensitive to the plugging strength of the conformance treatment materials. This observation was important for conformance treatment design in CCUS-EOR projects. According to this study, materials should reduce the channel permeability to make the KR below 30. The results demonstrate the importance of conformance treatment in maximizing the performance of CCUS-EOR process to achieve both oil recovery improvement and efficient carbon storage. This study provides guidelines for successful field applications of CO₂ transport control in CO₂ geo-utilization and storage.

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